

Amendment to the Claims:

This listing of claims will replace all prior versions, and listings, of claims in the application:

1. A gas phase olefin polymerization process comprising:
 - (1) preparing a solution of a catalyst precursor comprising a mixture of magnesium and titanium compounds, an electron donor and a solvent;
 - (2) adding a filler to the solution from step (1) to form a slurry;
 - (3) spray drying the slurry from step (2) at a temperature of 100 to 140°C to form a spray dried precursor;
 - (4) slurrying the spray dried precursor from step (3) in mineral oil,
 - (5) partially or fully pre-activating the catalyst precursor by contacting the slurry of step (4) with one or more Lewis Acids employing one or more in-line static mixers, and
 - (6) transferring the partially or fully activated precursor from step (5) under plug-flow conditions into a gas phase, olefin polymerization reactor and, if the precursor is partially preactivated, adding an activator to the reactor.
2. A gas phase olefin polymerization process comprising:
 - (1) preparing a solution of a catalyst precursor comprising a mixture of magnesium and titanium compounds, an electron donor and a solvent;
 - (2) adding a porous catalyst support, to the solution from step (1) to form a slurry;
 - (3) drying the slurry from step (2) to form a solid catalyst precursor;
 - (4) slurrying the solid precursor from step (3) in a viscous inert liquid,
 - (5) partially or fully pre-activating the catalyst precursor by contacting the slurry of step (4) with one or more Lewis Acids employing one or more in-line static mixers, and
 - (6) transferring the partially or fully activated precursor from step (5) under plug-flow conditions into a gas phase, olefin polymerization reactor and, if the precursor is partially preactivated, adding an activator to the reactor.
3. The process of Claim 1 or 2 wherein;
 - 1) the catalyst precursor in step (1) corresponds to the formula:
$$\text{Mg}_a(\text{M})(\text{OR})_e \text{X}_f (\text{ED})_g$$
wherein R is an aliphatic or aromatic hydrocarbon radical having 1 to 14 carbon atoms or COR' wherein R' is a aliphatic or aromatic hydrocarbon radical having 1 to 14 carbon atoms and each OR group is the same or different;

M is a transition metal;

X is independently chlorine, bromine or iodine;

ED is an electron donor;

d is 0.5 to 56; e is 0, 1, or 2; f is 2 to 116; g is >2 and up to $1.5(d) + 3$; and

2) the Lewis Acid of step (5) is

i) one or more compounds with formula $M'(R'')X_{(3-n)}$ wherein M' is aluminum or boron; each X is independently chlorine, bromine, or iodine; each R'' is independently a saturated aliphatic hydrocarbon radical having 1 to 14 carbon atoms, provided that when M is aluminum, n is 1 to 3 and when M is boron, n is 0 to 1.5; and

ii) is added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from 0.10:1 to 1.0:1.

4. The process of Claim 1 or 2, wherein said Lewis Acid is;

1) one or more alkylaluminum compound(s) with formula $M'(R'')X_{(3-n)}$ wherein M' is aluminum, R'' is n-butyl, n-hexyl, n-octyl, iso-octyl, isohexyl, and n-decyl, X is Cl or Br and n is a number from 0 to 1.5; and

2) added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from 0.10:1 to 0.75:1.

5. The process of Claim 4, wherein said Lewis Acid is;

1) selected from the group consisting triethylaluminum, tri-n-butyl aluminum, tri-n-hexyl aluminum, tri-n-octyl aluminum, tri n-decyl aluminum, triisoprenyl aluminum, dimethyl aluminum chloride, ethylaluminum dichloride, diethylaluminum chloride, and mixtures thereof; and

2) added in an amount such that the mole ratio of total Lewis Acid to electron donor in the precursor is from 0.10:1 to 0.30:1.

6. The process of Claim 4 wherein the slurry is partially or fully preactivated by first contacting with diethylaluminum chloride followed by tri-n-hexyl aluminum.

7. The process of Claim 1 or 2 wherein the viscosity of the slurry after addition of the activator or activators is adjusted to at least 1500 cP.

8. The process of Claim 1 or 2 in which the slurry of (2) is intimately mixed with the Lewis Acid by use of one or more vertically disposed staticmixers.

9. The process of claim 1 or 2 wherein the one or more static mixers and connecting piping have length/diameter ratios from 5 to 15.

10. The process of Claim 1 or 2 in which said gas phase reactor is the sole olefin polymerization reactor.

11. The process of Claim 1 or 2 wherein two olefin polymerization reactors are employed.